

8th International Berlin Workshop (IBW 8) on
Transport Phenomena with Moving Boundaries
25th - 26th October 2018, Berlin, Germany

Drop-based modelling of coalescence in batch settlers including polydispersity



Supported by:



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agenda

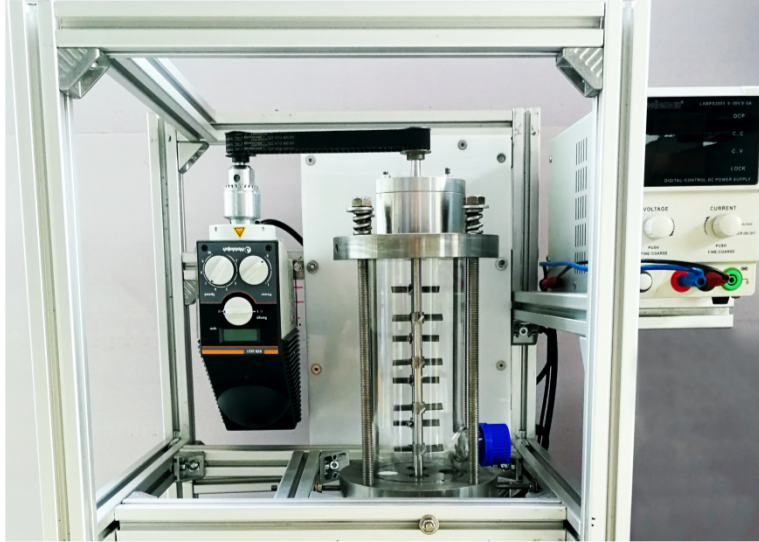
- settling experiment
- ReDrop concept
- coalescence model
- results



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settling cell

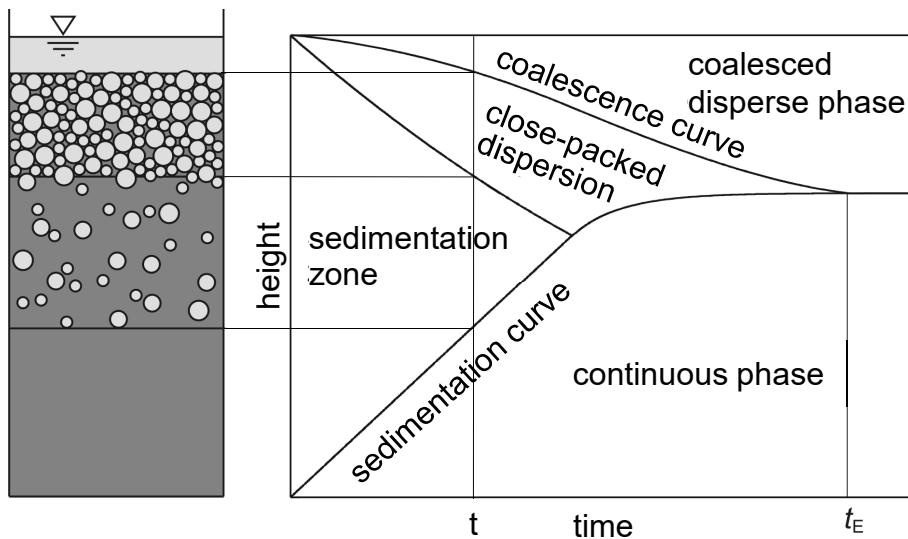


Leleu, Pfennig (2017). Standardized settling cell to characterize liquid-liquid dispersion. Proceedings of ISEC2017.

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principles of settling

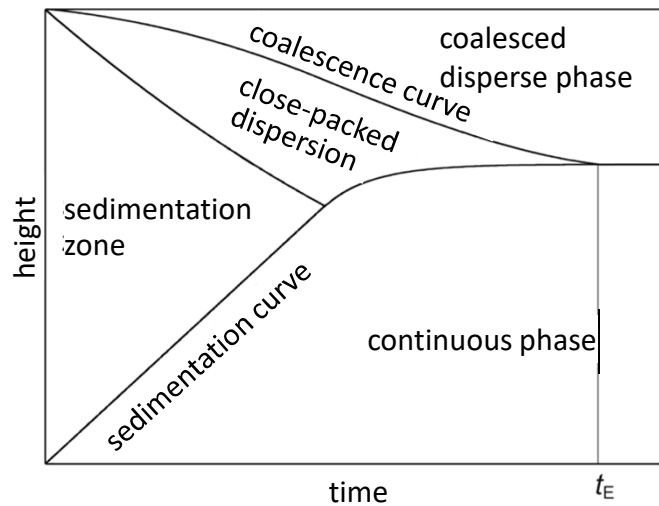


Henschke, Schlieper, Pfennig (2002). Determination of a coalescence parameter from batch-settling experiments. Chemical Engineering J., 85((2-3)), 369-378.

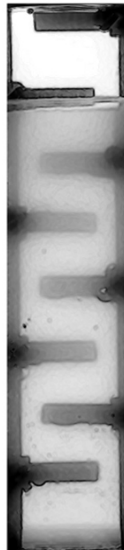
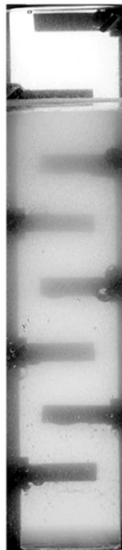
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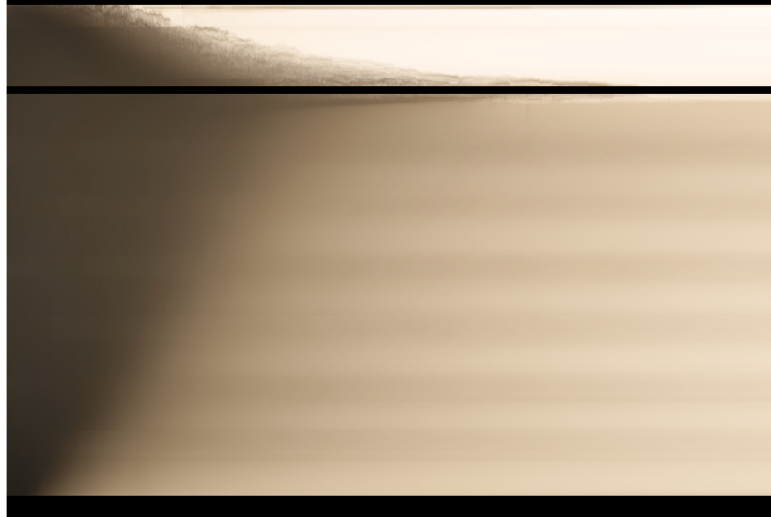
principles of settling



mask of the experiment

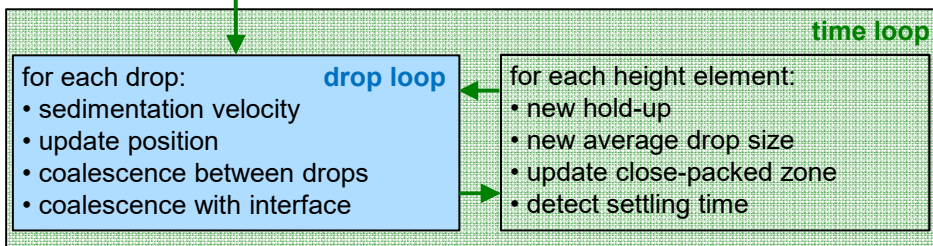


experiment evaluation

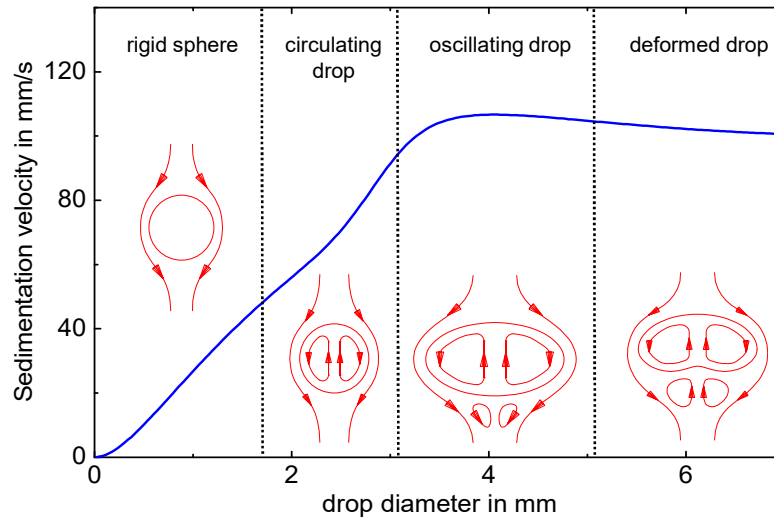


ReDrop = REpresentative DROPs

- initialization
- data input
- definition of height elements



single-drop sedimentation

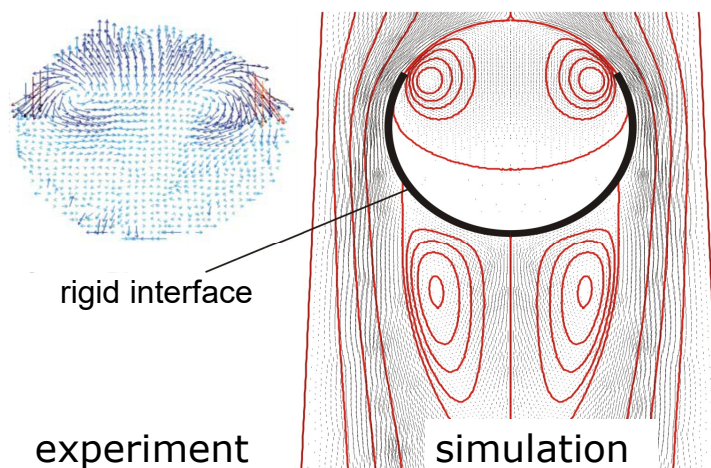


Kalem, Altunok, Pfennig (2010). Sedimentation behavior of droplets for the reactive extraction of zinc with D2EHPA. *AIChE Journal*, 56(1), 160-167.
 Waheed, Henschke, Pfennig (2004). Simulating sedimentation of liquid drops. *International Journal for Numerical Methods in Engineering*, 59(14), 1821-1837.

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comparison of simulation and experiment

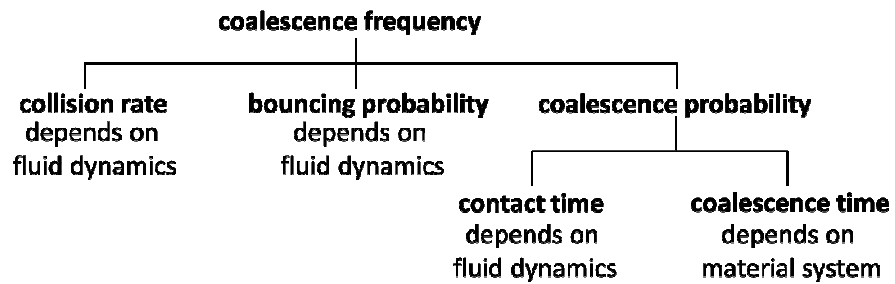


Gross-Hardt, Amar, Stapf, Blümich, Pfennig (2006). Flow dynamics measured and simulated inside a single levitated droplet. *Industrial and Engineering Chemistry*, 45(1), 416-423.

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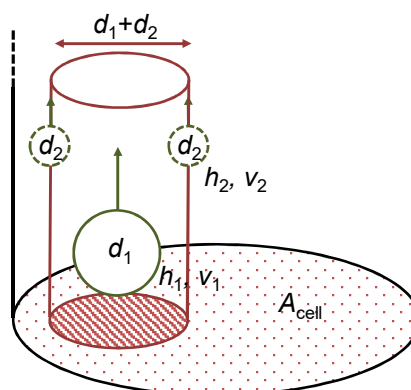


coalescence model



collision frequency

$$r_{\text{collision}} = \frac{A_{\text{collision}} / A_{\text{cell}}}{t_{\text{collision}}} = \frac{\pi(d_1 + d_2)^2 v_{\text{rel}}}{4A_{\text{cell}} |h_1 - h_2|}$$



free volume after Boublik and Mansoori

contact probability of two drops in polydisperse dispersion

$$g_{ij} = \frac{1}{1 - \xi_3} + \frac{6\xi_2 r_i r_j}{(1 - \xi_3)^2 (r_i + r_j)} + \frac{8\xi_2^2 r_i^2 r_j^2}{(1 - \xi_3)^3 (r_i + r_j)^2}$$

with

$$\xi_m = \frac{\pi N \sum_i x_i (2R_i)^m}{6V}$$

compare: dimensionless density after Carnahan & Starling

$$\eta = \frac{\pi N (2R)^3}{6V} = \varepsilon$$

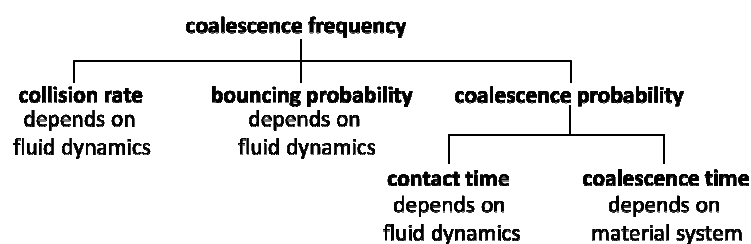


Kopriwa, Pfennig (2016). Characterization of Coalescence in Extraction Equipment Based on Lab-Scale Experiments. Solvent Extraction & Ion Exchange, 34(7), 622-642.

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Coulaloglou & Tavlarides



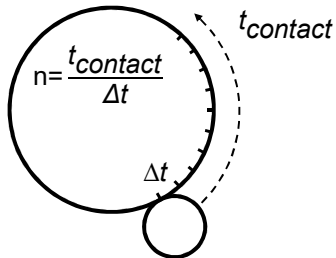
$$\omega = h (1 - p_{bouncing}) \exp\left(-\frac{t_{coalescence}}{t_{contact}}\right)$$



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coalescence probability



$$p_{non-coal, n\Delta t} = p_{non-coal, \Delta t}^n$$

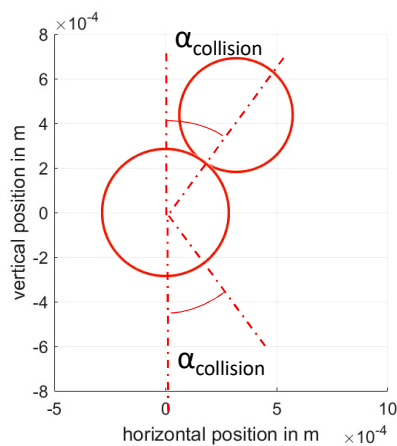
$$p_{non-coal, \Delta t} = \exp\left(-\frac{\Delta t}{t_{coalescence}}\right)$$

$$p_{non-coal, n\Delta t} = \exp\left(-\frac{n\Delta t}{t_{coalescence}}\right)$$

$$p_{non-coal} = \exp\left(-\frac{t_{contact}}{t_{coalescence}}\right)$$

$$p_{coal} = 1 - \exp\left(-\frac{t_{contact}}{t_{coalescence}}\right)$$

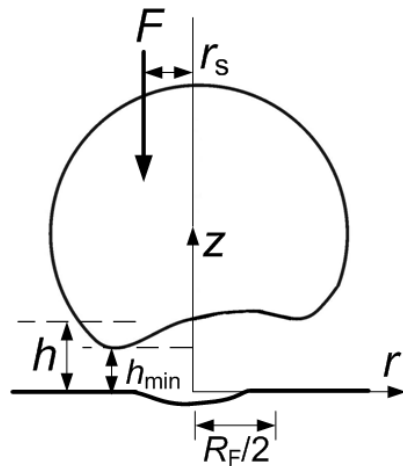
coalescence model: contact time



assumptions:

- drops follow contour during the sedimentation
- detachment angle = opposite of the collision angle

coalescence time, asymmetric dimple



$$t_{coalescence} = \frac{3\pi^{1.5}\mu R_{eq}^2}{4r_s^* \sqrt{\sigma F_{driving} h_{min}}}$$

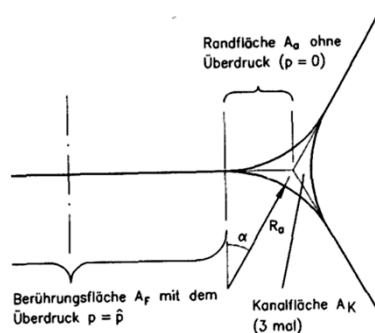
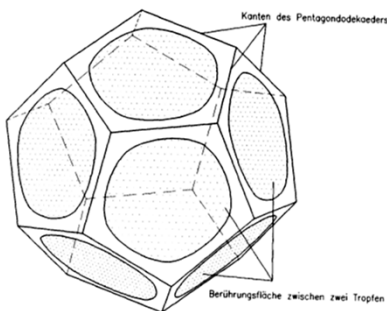


Henschke, Schlieper, Pfennig (2002). Determination of a coalescence parameter from batch-settling experiments. Chemical Engineering J., 85((2-3)), 369-378.
Pfennig, Schwerin (1995). Analysis of the Electrostatic Potential Difference in Aqueous Polymer 2-Phase Systems. Fluid Phase Equilibria, 108((1-2)), 305-315.

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dodecahedron deformation after Henschke

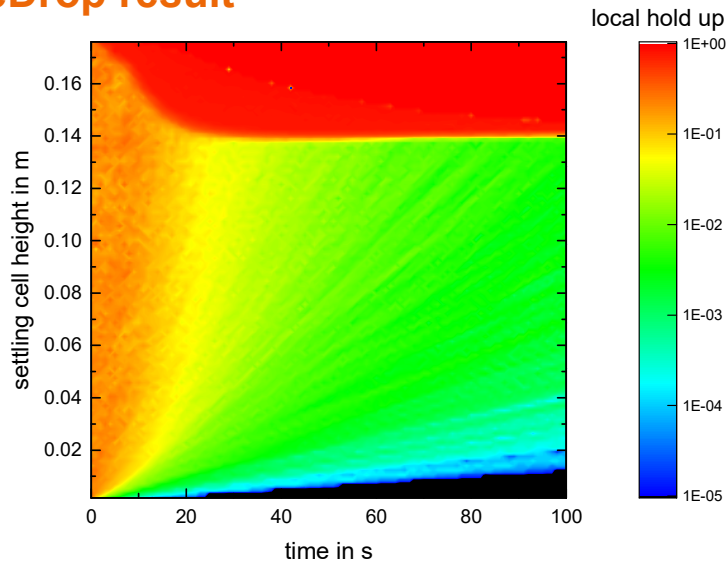


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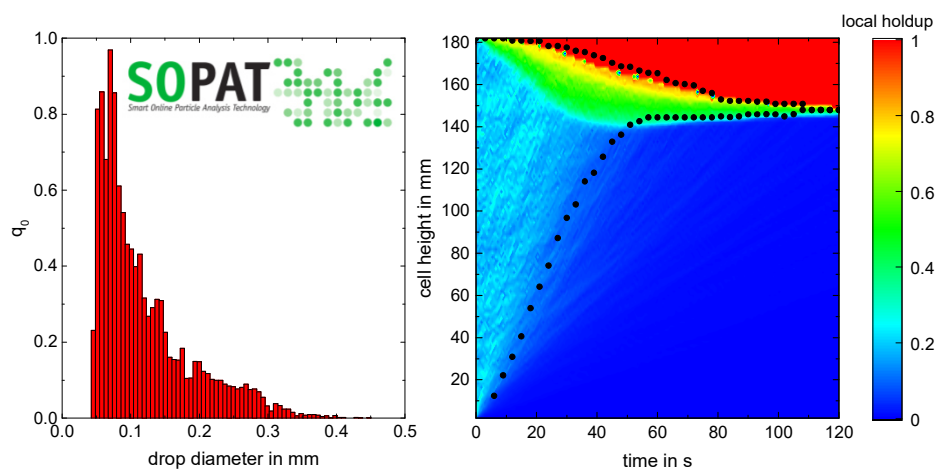
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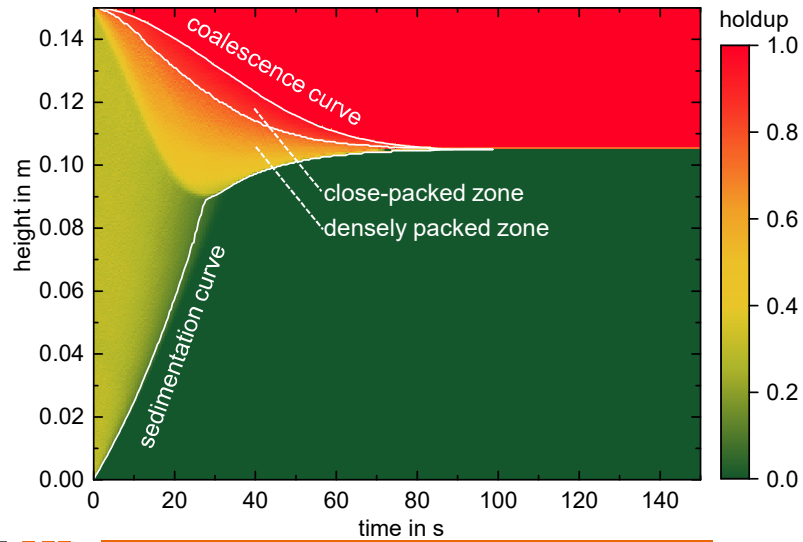
ReDrop result



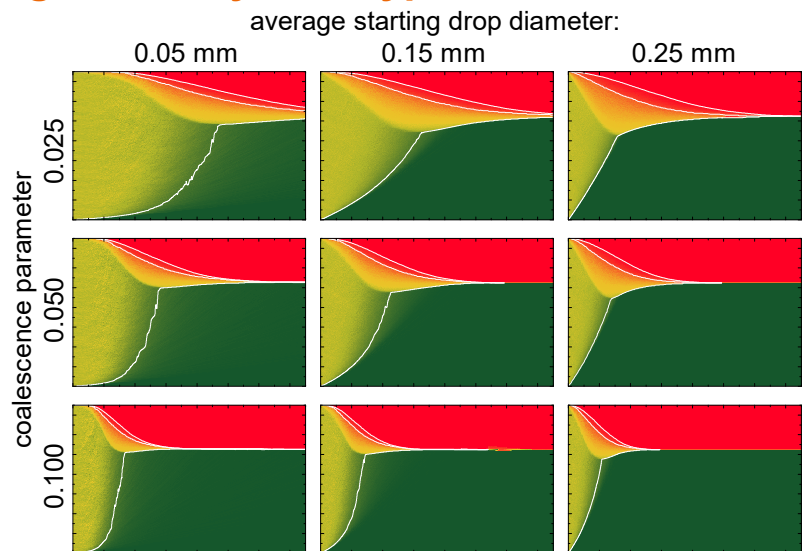
status of the model validation



ReDrop result



lag time & system-typical effective diameter



conclusions

- drop-based model → detailed results
- high-holdup flow → densely-packed zone
- sedimentation coalescence
 - lag time
 - system-typical effective diameter
- consistent modelling of coalescence



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